



RECEIVED  
JUL 25 2003  
TC 1700

09/889,497

VERIFICATION OF TRANSLATION

Re : Japanese Patent Application No. 11-009946

I, Sonoko TSUKIYAMA, of c/o Hosoda International Patent Office,  
OMM Building 5th Floor, P.O. Box 26, 1-7-31 Otemae, Chuo-ku, Osaka  
540-6591, JAPAN, hereby declare that I am the translator of the documents  
attached and certify that the following is a true translation of the best of my  
knowledge and belief.

Dated this 7th day of July, 2003

*Sonoko Tsukiyama*  
Sonoko TSUKIYAMA

(Seal)

PCT/JP00/00145

14.01.00

PATENT OFFICE

JAPANESE GOVERNMENT

This is to certify that the annexed is a true copy of the following application as  
filed with this Office.

Date of Application : January 18, 1999

Application Number : Japanese Patent Application

No. 11-009946

Applicant(s): Kao Corporation

[Document]	Petition for Patent Application
[File Number]	KAP98-0668
[Filing Date]	January 18, 1999
[Addressee]	Commissioner, Patent Office
[I.P.C.]	C11D 1/83
[Title of the Invention]	High-Density Detergent Composition
[Number of Claims]	4
[Inventor]	

[Address] c/o Kao Corporation, Research Laboratories,  
1334, Minato, Wakayama-shi

[Name] Shu YAMAGUCHI

[Inventor]

[Address] c/o Kao Corporation, Research Laboratories,  
1334, Minato, Wakayama-shi

[Name] Hideichi NITTA

[Inventor].

[Address] c/o Kao Corporation, Research Laboratories,  
1334, Minato, Wakayama-shi

[Name] Kyoko OKADA

[Inventor]

[Address] c/o Kao Corporation, Research Laboratories,  
1334, Minato, Wakayama-shi

[Name] Kimihiro MIZUSAWA

[Inventor]

[Address] c/o Kao Corporation, Research Laboratories,  
1334, Minato, Wakayama-shi

[Name] Jun KOZUKA

[Inventor]

[Address] c/o Kao Corporation, Research Laboratories,  
1334, Minato, Wakayama-shi

[Name] Hiroyuki YAMASHITA

[Applicant]

[Identification Number] 000000918

[Name] Kao Corporation

[Proxy]

[Identification Number] 100095832

[Patent Attorney]

[Name] Yoshinori HOSODA

[Indication of Official Fee]

[Register Number for Prepayment] 050739

[Amount of Payment] 21,000 yen

[List of Annexed Documents]

[Document] Specification 1

[Document] Drawings 1

[Document] Abstract 1

[Number of General Authorization] 9200353

[Requirement of Proof] Required

[Document] Specification

[Title of the Invention] High-Density Detergent Composition

[Claims]

[Claim 1] A high-density detergent composition comprising 10 to 60% by weight of a surfactant composition having a weight ratio of an anionic surfactant to a nonionic surfactant of 4:10 or more and 10:0 or less, the high-density detergent composition having a bulk density of from 600 to 1200 g/L, wherein the high-density detergent composition has a total summation of a product of a mass base frequency  $W_i$  of each group of classified granules obtained by classifying detergent granules by using a classifier and a dissolving rate  $V_i$  of each group of classified granules, which satisfies the following formula (A):

$$\Sigma(W_i \bullet V_i) \geq 95(\%) \quad (A)$$

and wherein a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.1 or less, wherein the classifier comprises sieves each having a sieve-opening 2000  $\mu\text{m}$ , 1410  $\mu\text{m}$ , 1000  $\mu\text{m}$ , 710  $\mu\text{m}$ , 500  $\mu\text{m}$ , 355  $\mu\text{m}$ , 250  $\mu\text{m}$ , 180  $\mu\text{m}$ , and 125  $\mu\text{m}$ , and a receiver, and the dissolving rate  $V_i$  is determined under the following measurement conditions:

supplying  $1.000 \text{ g} \pm 0.010 \text{ g}$  of a sample to  $1.00 \text{ L} \pm 0.03 \text{ L}$  of water at  $5^\circ\text{C} \pm 0.5^\circ\text{C}$  having a water hardness of  $4^\circ\text{DH}$ , stirring in a 1 L beaker of which inner diameter is 105 mm, with a cylindrical stirring rod of which length is 35 mm and diameter is 8 mm, at a rotational speed of 800 rpm for 120 seconds, and thereafter filtering insoluble remnants by a standard sieve having a sieve-opening of 300  $\mu\text{m}$  as defined according to JIS Z 8801, wherein the dissolving rate  $V_i$  of the classified granules is calculated by the following formula (a), i

being each group of the classified granules:

$$V_i = (1 - T_i/S_i) \times 100(\%) \quad (a)$$

wherein  $S_i$  is a weight (g) of each group of the classified granules supplied; and  $T_i$  is a dry weight (g) of the insoluble remnants of each group of the classified granules remaining on the sieve after filtration.

[Claim 2] A high-density detergent composition comprising 10 to 60% by weight of a surfactant composition having a weight ratio of an anionic surfactant to a nonionic surfactant of 0:10 or more and less than 4:10, the detergent composition having a bulk density of from 600 to 1200 g/L, wherein the high-density detergent composition has a total summation of a product of a mass base frequency  $W_i$  of each group of classified granules obtained by classifying detergent granules by using the classifier as defined in claim 1 and a dissolving rate  $V_i$  of each group of the classified granules determined under the measurement conditions as defined in claim 1, which satisfies the following formula (B):

$$\Sigma(W_i \cdot V_i) \geq 97(\%) \quad (B)$$

and wherein a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.08 or less.

[Claim 3] A process for preparing the high-density detergent composition of claim 1, comprising subjecting unclassified detergent granules comprising 10 to 60% by weight of a surfactant composition to classification operation; and adjusting a particle size of each group of the resulting classified granules, such that the formula (A) as defined in claim 1 is satisfied, and that a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.1 or less.

[Claim 4] A process for preparing the high-density detergent composition of claim 2, comprising subjecting unclassified detergent granules comprising 10 to 60% by weight of a surfactant composition to classification operation; and adjusting a particle size of each group of the resulting classified granules, such that the formula (B) as defined in claim 2 is satisfied, and a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.08 or less.

[Detailed Description of the Invention]

[0001]

[Technical Field to Which the Invention Pertains]

The present invention relates to a high-density detergent composition and a process for preparing the same.

[0002]

[Prior Art]

While increasing the density of the powdery detergent composition has imparted great advantages in the improvement in the transportation efficiency and the convenience in the users, there is an increasing concern on the dissolubility by compression of the detergent granules.

While since the mid 1990's, the washing machines have the tendency of having large volume capacity and water conservation by the demands of users, and short-period washing mode or gentle stirring mode meeting the demands of reduction in clothes damaging has been set. However, in either of the modes, the amount of work (i.e. mechanical power  $\times$  time) of the washing machine tends to be lowered. As a result, there arise crucial problems that the dissolubility of the detergent granules is drastically lowered, so that the detergency becomes poor

and that the insoluble remnants deposit on clothes.

On the other hand, Japanese Unexamined Patent Publication No. Hei 7-509267 discloses a detergent composition comprising a base powder comprising granules having a size of less than 150  $\mu\text{m}$  in an amount of less than 10% by weight, and granules having a size exceeding 1700  $\mu\text{m}$  in an amount of less than 10% by weight; and filler granules made of sodium citrate, sodium hydrogencarbonate, or the like. However, the detergent composition does not sufficiently solve the problems relating to the dissolubility and the dispersibility of the detergent composition in a case where the amount of work of the washing machine is low.

[0003]

#### [Problems to Be Solved by the Invention]

An object of the present invention is to provide a high-density detergent composition which is excellent in the detergency even when the amount of work of the washing machine is low, and excellent in the dissolubility of the granules and the dispersibility.

[0004]

#### [Means to Solve the Problems]

Specifically, the present invention relates to:

- (1) a high-density detergent composition (hereinafter referred to as "Detergent Composition I") comprising 10 to 60% by weight of a surfactant composition having a weight ratio of an anionic surfactant to a nonionic surfactant of 4:10 or more and 10:0 or less, the high-density detergent composition having a bulk density of from 600 to 1200 g/L, wherein the high-density detergent composition has a total summation of a product of a mass base



frequency  $W_i$  of each group of classified granules obtained by classifying detergent granules by using a classifier and a dissolving rate  $V_i$  of each group of classified granules, which satisfies the following formula (A):

$$\Sigma(W_i \bullet V_i) \geq 95(\%) \quad (A)$$

and wherein a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.1 or less, wherein the classifier comprises sieves each having a sieve-opening 2000  $\mu\text{m}$ , 1410  $\mu\text{m}$ , 1000  $\mu\text{m}$ , 710  $\mu\text{m}$ , 500  $\mu\text{m}$ , 355  $\mu\text{m}$ , 250  $\mu\text{m}$ , 180  $\mu\text{m}$ , and 125  $\mu\text{m}$ , and a receiver (hereinafter referred to as “classifier”), and the dissolving rate  $V_i$  is determined under the following measurement conditions (hereinafter referred to as “measurement conditions for dissolution”):

supplying  $1.000 \text{ g} \pm 0.010 \text{ g}$  of a sample to  $1.00 \text{ L} \pm 0.03 \text{ L}$  of water at  $5^\circ\text{C} \pm 0.5^\circ\text{C}$  having a water hardness of  $4^\circ\text{DH}$ , stirring in a 1 L beaker of which inner diameter is 105 mm, with a cylindrical stirring rod of which length is 35 mm and diameter is 8 mm, at a rotational speed of 800 rpm for 120 seconds, and thereafter filtering insoluble remnants by a standard sieve having a sieve-opening of 300  $\mu\text{m}$  as defined according to JIS Z 8801, wherein the dissolving rate  $V_i$  of the classified granules is calculated by the following formula (a),  $i$  being each group of the classified granules:

$$V_i = (1 - T_i/S_i) \times 100(\%) \quad (a)$$

wherein  $S_i$  is a weight (g) of each group of the classified granules supplied; and  $T_i$  is a dry weight (g) of the insoluble remnants of each group of the classified granules remaining on the sieve after filtration; and a process for preparing the same; and

(2) high density polyethylene composition (hereinafter referred to as

“Detergent Composition II”) comprising 10 to 60% by weight of a surfactant composition having a weight ratio of an anionic surfactant to a nonionic surfactant of 0:10 or more and less than 4:10, the detergent composition having a bulk density of from 600 to 1200 g/L, wherein the high-density detergent composition has a total summation of a product of a mass base frequency  $W_i$  of each group of classified granules obtained by classifying detergent granules by using the classifier as defined above and a dissolving rate  $V_i$  of each group of the classified granules determined under the measurement conditions as defined above, which satisfies the following formula (B):

$$\Sigma(W_i \cdot V_i) \geq 97(\%) \quad (B)$$

and wherein a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.08 or less; and a process for preparing the same.

Here, the term “mass base frequency” refers to a value obtained by dividing the weight of the classified granules on each sieve or on the receiver by an entire weight of the detergent composition, the classified granules being obtained by classifying the detergent granules with a classifier.

[0005]

[Modes for Carrying out the Invention]

[1] Composition

The surfactant composition in the detergent composition of the present invention has a content of from 10 to 60% by weight, preferably from 20 to 50% by weight, more preferably from 27 to 45% by weight, of the detergent composition, from the viewpoints of obtaining the detergency and the desired powder properties of the detergent composition. The surfactant composition comprises an anionic surfactant and/or a nonionic surfactant, and may also

comprise a cationic surfactant and an amphoteric surfactant as occasion demands.

The anionic surfactants include alkylbenzenesulfonates, alkyl or alkenyl ether sulfates, alkyl or alkenyl sulfates,  $\alpha$ -olefinsulfonates,  $\alpha$ -sulfofatty acid salts or esters thereof, alkyl or alkenyl ether carboxylates, salts of fatty acids, and the like. The anionic surfactant has a content of preferably from 1 to 50% by weight, more preferably from 5 to 30% by weight of the detergent composition, from the viewpoint of the detergency.

[0006]

As the counter ions for the anionic surfactants, the alkali metal ions are preferable from the viewpoint of improvement in the detergency. Especially, potassium ions are preferable, from the viewpoint of the improvement in the dissolution rate. The potassium ions are contained in an amount of preferably 5% by weight or more, more preferably 20% by weight or more, particularly preferably 40% by weight or more in the entire counter ions.

The anionic surfactant in the form of potassium salt is prepared by a process for neutralizing an acid precursor of the corresponding anionic surfactant with an alkalizing agent such as potassium hydroxide or potassium carbonate; a process of carrying out cationic exchange by allowing to coexist in the detergent granules a salt of the anionic surfactant other than the potassium salt and potassium carbonate; and the like.

[0007]

The nonionic surfactants include polyoxyalkylene alkyl ethers, polyoxyalkylene alkylphenyl ethers, polyoxyalkylene fatty acid esters, polyoxyethylene- polyoxypropylene alkyl ethers, polyoxyalkylene alkylamines, glycerol fatty acid esters, higher fatty acid alkanolamides, alkylglycosides,

alkylglucosamides, alkylamine oxides, and the like. From the viewpoint of detergency, polyoxyalkylene alkyl ethers are preferable, which are ethylene oxide adducts, or a mixture adduct of ethylene oxide and propylene oxide, each of which alcohol moiety has 10 to 18 carbon atoms, preferably 12 to 14 carbon atoms, the average moles of each alkylene oxide being 5 to 30, preferably 6 to 15.

In addition, the polyoxyethylene-polyoxypropylene-polyoxyethylene alkyl ether is preferable, from the viewpoints of the detergency and the dissolubility. The compound can be obtained by reacting an ethylene oxide adduct of which alcohol moiety has 10 to 18 carbon atoms, preferably 12 to 14 carbon atoms with propylene oxide and subsequently with ethylene oxide. Further, among the polyoxyethylene alkyl ethers mentioned above, those having a narrow alkylene oxide distribution are preferable. The compound can be obtained by using a magnesium catalyst described in Japanese Patent Laid-Open No. Hei 7-227540 and the like.

The nonionic surfactant has a content of preferably from 1 to 50% by weight, more preferably from 5 to 30% by weight, of the detergent composition, from the viewpoint of the detergency.

The cationic surfactants include alkyl trimethylammonium salts, and the like, and the amphoteric surfactants include carbobetain-type and sulfobetain-type surfactants, and the like.

[0008]

In the detergent composition of the present invention, there can be formulated with water-soluble inorganic salts such as carbonates, hydrogencarbonates, silicates, sulfates, sulfites, and salts of phosphoric acids. Here, the carbonate is contained, calculated on the basis of an anhydride, in an

amount of preferably 25% by weight or less, more preferably from 5 to 20% by weight, particularly preferably from 7 to 15% by weight, of the detergent composition, and a total sum of the carbonate and the sulfate, calculated on the basis of an anhydride, in an amount of preferably from 5 to 35% by weight, more preferably from 10 to 30% by weight, particularly preferably from 12 to 25% by weight, of the detergent composition, from the viewpoints of the detergency and the low-temperature dispersibility under the conditions of allowing the detergent composition to stand in cold water for a long period of time.

[0009]

In the detergent composition of the present invention, crystalline silicates can be formulated. The  $\text{SiO}_2/\text{M}_2\text{O}$  molar ratio (wherein M is an alkali metal atom) is preferably 0.5 or more, from the viewpoints of the metal ion capturing ability and the anti-hygroscopic property, and the molar ratio is preferably 2.6 or less, from the viewpoint of the alkalizing ability. The molar ratio is particularly preferably from 1.5 to 2.2. It is preferable to formulate a crystalline silicate having an average particle size of from about 1 to about 40  $\mu\text{m}$ , from the viewpoints of the fast dissolubility and the powder properties, and its content is preferably from 0.5 to 40% by weight, more preferably from 1 to 25% by weight, of the detergent composition, from the viewpoints of the powder properties and the detergency after storage. Especially, its combined use with sodium carbonate is preferable.

In addition, in the detergent composition of the present invention, it is preferable to formulate a cationic exchange-type polymer having carboxylic acid group and/or sulfonic acid group, from the viewpoint of the metal ion capturing capacity and the dispersibility of the solid particle stains. Especially, desirable

are salts of acrylic acid-maleic acid copolymers having a molecular weight of 1000 to 80000; polyacrylates; and salts of polyacetal carboxylic acids such as polyglyoxylic acid having a molecular weight of 800 to 1000000, preferably from 5000 to 200000 described in Japanese Patent Laid-Open No. Sho 54-52196.

The cationic exchange-type polymer is contained in an amount of preferably from 0.5 to 12% by weight, more preferably from 1 to 7% by weight, particularly preferably from 2 to 5% by weight, of the detergent composition, from the viewpoint of the detergency.

[0010]

In addition, the crystalline aluminosilicate such as A-type, X-type, or P-type zeolite can be formulated, and the average primary particle size is preferably from 0.1 to 10  $\mu\text{m}$ . Also, an amorphous aluminosilicate having an oil-absorbing capacity of 80 mL/100 g or more as determined by the method in accordance with JIS K 5101 can be formulated, for the purpose of preventing bleeding out of the liquid components such as the nonionic surfactant. As the amorphous aluminosilicates, for instance, there may be referred to Japanese Patent Laid-Open Nos. Sho 62-191417, Sho 62-191419, and the like. The amorphous aluminosilicate has a content of preferably from 0.1 to 20% by weight of the detergent composition.

[0011]

The detergent composition of the present invention can be formulated with organic acid salts such as citrates and ethylenediaminetetraacetate; dispersing agents or dye-transfer inhibitors such as carboxymethyl cellulose, polyethylene glycols, polyvinyl pyrrolidones and polyvinyl alcohols; bleaching agents such as percarbonates; bleaching activators such as compounds listed in

Japanese Patent Laid-Open No. Hei 6-316700 and tetraacetythylenediamine; enzymes such as protease, cellulase, amylase, and lipase; biphenyl-type or stilbene-type fluorescent dyes; defoaming agents; antioxidants; blueing agents; perfumes, and the like. Incidentally, granules prepared by separately granulating an enzyme, a bleaching activator, a defoaming agent, and the like may be after-blended.

[0012]

[2] Bulk Density

The bulk density of the detergent composition determined in accordance with JIS K3362 is from 600 to 1200 g/L. From the viewpoints of improvement in the transportation efficiency and the convenience of the users, the bulk density is 600 g/L or more, preferably 650 g/L or more, more preferably 700 g/L or more. From the viewpoint of keeping the void between the granules and improving the dispersibility owing to the suppression of the increase in number of contact between the granules, the bulk density is 1200 g/L or less.

[0013]

[3] Particle Size Distribution

The detergent composition of the present invention is excellent in the dissolubility per one granule of the detergent granules and the prevention of forming aggregation of the detergent granules. Here, the aggregation of the detergent granules refers to a phenomenon where after initiation of dissolving a part of a surfactant capable of forming liquid crystals and an inorganic salt forming hydrated crystals of carbonates, sulfates and the like, the remainder part forms highly viscous liquid crystals between the detergent granules or recrystallizes into a hydrate more quickly than being dissolved. Therefore, from

the viewpoint of the prevention of forming aggregation of the detergent granules, the particle size distribution of the detergent composition of the present invention is such that the mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  in the detergent composition I or II is 0.1 or less or 0.08 or less, respectively.

[0014]

From the viewpoints of improvements in the low-temperature dispersibility and the flowability, it is preferable that the content of the fine powder in the detergent composition is small. The mass base frequency of the classified granules having a particle size of less than 125  $\mu\text{m}$  is such that in the detergent composition I, the mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.1 or less, preferably 0.08 or less, more preferably 0.06 or less, particularly preferably 0.05 or less, and that in the detergent composition II, the mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.08 or less, preferably 0.06 or less, more preferably 0.04 or less. In addition, the mass base frequency of the classified granules having a particle size of 125  $\mu\text{m}$  or more and less than 180  $\mu\text{m}$  in both the detergent compositions I and II is preferably 0.20 or less, more preferably 0.10 or less, particularly preferably 0.05 or less. Here, regarding the fine powder, it is preferable that each mass base frequency satisfies the relationship such that the mass base frequency of [classified granules having a particle size of less than 125  $\mu\text{m}$ ]  $\leq$  [classified granules having a particle size of 125  $\mu\text{m}$  or more and less than 180  $\mu\text{m}$ ].

[0015]

In addition, from the viewpoint of fast dissolubility per one granule, it is



preferable that the content of the coarse granules in both the detergent compositions I and II is small. Specifically, the mass base frequency of the classified granules having a particle size of 1000  $\mu\text{m}$  or more is preferably 0.03 or less, more preferably 0.01 or less, particularly preferably substantially none. The mass base frequency of the classified granules having a particle size of 710  $\mu\text{m}$  or more and less than 1000  $\mu\text{m}$  is preferably 0.10 or less, more preferably 0.05 or less, particularly preferably 0.03 or less. The mass base frequency of the classified granules having a particle size of 500  $\mu\text{m}$  or more and less than 710  $\mu\text{m}$  is 0.10 or less, preferably 0.05 or less, more preferably 0.03 or less. Here, regarding the coarse granules, it is preferable that each mass base frequency satisfies the relationship such that the mass base frequency of [classified granules having a particle size of 1000  $\mu\text{m}$  or more]  $\leq$  [classified granules having a particle size of 710  $\mu\text{m}$  or more and less than 1000  $\mu\text{m}$ ]  $\leq$  [classified granules having a particle size of 500  $\mu\text{m}$  or more and less than 710  $\mu\text{m}$ ].

[0016]

The detergent composition of the present invention has an average particle size of preferably from 150  $\mu\text{m}$  to 500  $\mu\text{m}$ , more preferably from 200  $\mu\text{m}$  to 400  $\mu\text{m}$ , particularly preferably from 250  $\mu\text{m}$  to 350  $\mu\text{m}$ . Here, the average particle size ( $D_p$ ) is a 50% mass base diameter, and can be determined by using the classifier mentioned above. Specifically, after classification operation, the mass base frequency is accumulated sequentially from finer powders to coarser granules. When a sieve-opening of a first sieve of which cumulative mass base frequency is 50% or more is defined as a  $\mu\text{m}$ , and a sieve-opening of one sieve-opening larger than a  $\mu\text{m}$  is defined as b  $\mu\text{m}$ , in a case where the cumulative

mass base frequency from the receiver to the a  $\mu\text{m}$ -sieve is defined as c%, and the mass base frequency of granules on the a  $\mu\text{m}$ -sieve is defined as d%, the average particle size can be calculated according to the equation (b).

$$D_p = 10^A \quad (b)$$

wherein  $A = [50 - (c - d/(\log b - \log a) \times \log b)]/[d/(\log b - \log a)]$

[0017]

#### [4] Dissolubility of Classified Granules

In the determination of the dissolubility of each group of the classified granules, first a sample accurately weighed by using, for example, an electronic balance "Model ER-180A" manufactured by Kensei Kogyo K.K. is supplied evenly so as not to cause aggregation of the granules and stirred, and thereafter filtered with a standard sieve defined by JIS Z 8801 (sieve-opening: 300  $\mu\text{m}$ ) [the sieve having a sieve area of 35  $\text{cm}^2$  or more and a weight within 10 g is used, and the weight is previously measured]. Subsequently, the insoluble remnants of each group of the classified granules remained on the sieve are subjected to drying operation together with the sieve for 1 hour in an electric dryer at 105°C, and allowed to cool for 30 minutes in a desiccator (25°C) containing an activated silica gel therein. Thereafter, the weight is determined. By subtracting the weight of the sieve from this determined weight, the dry weight of the insoluble remnants of each group of the classified granules can be calculated.

[0018]

The concrete determination conditions are as described as the conditions for dissolubility determination described above. Here, the sieve-opening of 300  $\mu\text{m}$  is roughly corresponding to a pore size of a lint filter attached to the washing machine, which means that the high-density detergent composition

which satisfies the above-mentioned conditions can pass through the lint filter in a very short period of time even with a water temperature of 5°C. This means that this detergent composition can satisfactorily meet the requirements for short time washing modes of the recent washing machines.

[0019]

[5] Dissolubility of Detergent Composition

The dissolubility of the detergent composition of the present invention is expressed by a total summation of a product of a mass base frequency  $W_i$  of each group of the classified granules and a dissolving rate  $V_i$  of each group of the classified granules [namely  $\Sigma(W_i \cdot V_i)$ ]. The dissolubility of the detergent composition I is 95% or more, preferably 97% or more, more preferably 98% or more, and the dissolubility of the detergent composition II is 97% or more, preferably 98% or more, more preferably 99% or more.

Since the detergent composition of the present invention has extremely high dissolubility markedly distinctive from those of conventional detergent compositions even under cold water conditions, the probability of causing insoluble remnants even washing under the conditions of super-low mechanical power is extremely low, aside from having such effects that the detergency is increased by eluting the deterging components more quickly in the washtub.

[0020]

[6] Flowability

When the detergent composition of the present invention is placed in a washing machine, it is preferable that its flowability is excellent (more likely to be evenly dispersed) in order to alleviate the lowering of the dispersibility when the composition is in contact with water in a case where the composition is

locally gathered together. The flow time (a time period required for dropping 100 mL of powder from a hopper used in a measurement of bulk density according to JIS K 3362) is preferably 10 seconds or shorter, more preferably 8 seconds or shorter, still more preferably 6.5 seconds or shorter.

[0021]

[7] Preparation Process

The detergent composition of the present invention can be prepared by subjecting unclassified detergent granules, comprising 10 to 60% by weight of a surfactant composition, to classification operation and particle size adjustment operation (the detergent granules being hereinafter also referred to as “base detergent granules”; here, classified granules obtained by subjecting base detergent granules to a plural times of classification operation and operation for particle size adjustment may be also included in the base detergent granules).

[0022]

(Step 1-1) Preparation Step of Base Detergent Granules of Detergent Composition I

As one embodiment of the process for preparing base detergent granules usable in the detergent composition I, there can be employed a process comprising preparing spray-dried particles comprising a surfactant and a builder, and increasing bulk density; and the like. Such a process includes, for instance, a process comprising stirring and granulating spray-dried particles in a vertical or horizontal mixer, thereby increasing the bulk density; and the like. As examples of such processes, there can be employed a process disclosed in Japanese Patent Laid-Open No. Sho 61-69897, comprising stirring and granulating spray-dried particles; a process disclosed in Japanese Patent Laid-Open No. Sho 62-169900,

comprising forming dried particles, and thereafter disintegrating and granulating the dried particles; a process disclosed in Japanese Patent Laid-Open No.

Sho 62-236897, comprising disintegrating a solid detergent obtained by kneading and mixing detergent raw materials; from the viewpoint of energy saving, as a process without using a spray-drying tower, a process disclosed in Japanese Patent Laid-Open No. Hei 3-33199, comprising neutralizing in a dry state an acid precursor of an anionic surfactant with a granular, solid alkalizing agent in a high-speed mixer, and thereafter adding a liquid binder to form granules; and the like.

[0023]

(Step 1-2) Preparation Step of Base Detergent Granules of Detergent Composition II

As one embodiment of the process for preparing base detergent granules usable in the detergent composition II, there can be employed a process disclosed in Japanese Patent Laid-Open No. Hei 10-176200, comprising granulating a mixture comprising a nonionic surfactant, an acid precursor of an anionic surfactant capable of having a lamellar orientation, and an alkalizing agent, while tumbling with a granulator at a temperature not less than the temperature capable of neutralizing the mixture, and the like.

[0024]

(Step 2) Classification Step and Particle Size Adjustment Step

The base detergent granules are subjected to classification and particle size adjustment, whereby the detergent composition of the present invention can be obtained. The classification method includes a method employing a circular or sectoral vibration sieve; an ultrasonic vibration sieve comprising the vibration

sieve and an ultrasonic oscillator attached thereto; an air classifier or centrifugal classifier, and the like.

The detergent composition I can be obtained by subjecting base detergent granules to at least one step of classification operation; thereafter determining a mass base frequency for each group of sieve-on classified granules and sieve-pass classified granules against an amount of the base detergent granules supplied; and blending each group of classified granules such that the formula (A) as defined above is satisfied, and that a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.1 or less. Similarly, the detergent composition II can be obtained by blending each group of classified granules such that the formula (B) as defined above is satisfied, and that a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.08 or less.

Incidentally, the classification operation may be single-step operation as shown in Figure 1 (1), or two or more steps of operations as shown in Figure 1 (2) as occasion demands. A desired detergent composition can be obtained, for instance, by separating coarse granules in the first-step classification operation, from the viewpoint of the fast dissolubility per one granule; separating fine powder, for instance, classified granules having a size of less than 125  $\mu\text{m}$ , in the second-step classification operation, from the viewpoint of the low-temperature dispersibility; and subjecting a part or entire fine powder to granulation operation to be supplied again to the base detergent granules. As the blending method, there can be employed a blending method in a batch process with a V-type mixer, or the like, or continuous process.

[0025]

In addition, the detergent composition can be obtained in a high yield by granulating and/or disintegrating the base detergent granules which are excess base detergent granules not subjected to particle size adjustment; and thereafter reusing as the base detergent granules. In other words, those granules, like fine powder having a size of less than 125  $\mu\text{m}$ , having excellent dissolubility per one granule but having a concern for decreasing the dispersibility of the detergent composition by an increase in the number of contact between the granules can be reused as base detergent granules after subjecting to a treatment for increasing particle size such as granulation operation. It is especially important for the detergent composition of the present invention that the mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is reduced, and the process becomes economically advantageous by carrying out the above operations. On the other hand, excess coarse granules which are poor in the dissolubility per one granule can be reused as base detergent granules after subjecting the coarse granules to a treatment for decreasing particle size such as disintegration operation.

Specifically, in the detergent composition I, the classified granules not used in Steps 1-1 or 1-2 and 2 mentioned above can be preferably reused as base detergent granules in reference to the dissolving rate  $V_i$ , in a case where, for instance, fine powder having  $V_i$  of 95% or more is subjected to granulation operation, or coarse granules having  $V_i$  of less than 95% are subjected to disintegration operation. Similarly, in the detergent composition II, fine powder having  $V_i$  of 97% or more is subjected to granulation operation, or coarse granules having  $V_i$  of less than 97% are subjected to disintegration operation, whereby the granules are preferably reused as base detergent granules. The fine

powder granulation operation and the coarse granules disintegration operation are exemplified below.

[0026]

(Fine Powder Granulation Operation)

Excess fine powder may be collected by adding them in the form of fine powder during the preparation process of Step 1-1 or 1-2 for the base detergent granules. In addition, as an alternative collecting method, for instance, the excess fine powder may be collected by a process comprising compressing and granulating in a vertical or horizontal granulator; an extruding granulation process employing an extruder; a compression-granulation method such as briquetting, and the like. In addition, a binder can be added during granulation.

[0027]

(Coarse Granules Disintegration Step)

Excess coarse granules can be reused as base detergent granules by, for instance, disintegrating the coarse granules, thereby decreasing their particle size. The disintegrator for coarse granules includes impact crushers such as hammer crusher; impact pulverizers such as atomizers and pin mills; shearing rough pulverizers such as flash mills. These disintegrators may comprise single-step operation, or multi-step operations with the same or different disintegrators. Incidentally, it is preferable to add fine powder as an agent for controlling deposition within devices or as a surface-modifying agent for pulverized surfaces. The fine powder is preferably inorganic powders such as aluminosilicates, silicon dioxide, bentonite, talc and clay amorphous silica derivatives, and especially, crystalline or amorphous aluminosilicates are preferable. In addition, fine powders of inorganic salts such as sodium carbonate and sodium sulfate can



be used.

In addition, for the purpose of coating and smoothening a surface-modifying agent for improving flowability of the disintegrated granules, a surface-modifying step can be provided in the process. For instance, there may be employed the process comprising supplying a composition in a batch process or continuous process into a rotatable cylindrical mixer or an agitator, thereby subjecting the composition to tumbling or stirring treatment.

[0028]

By the combination of the fine powder granulation operation and the coarse granules disintegration operation, the detergent composition can be obtained in a high yield from the excess classified detergent granules in Step 2. In addition, after the classification and particle size adjustment steps, there can be formulated enzymes, dyes, perfumes, and the like.

[0029]

[Examples]

Evaluation 1 [Dissolubility of Detergent] A lint filter (model number: AXW22A-5RU0, pore-size:  $300 \times 640 \mu\text{m}$ ) was attached to a side wall portion of a washtub of a washing machine "AISAIGO NA-F70VP1" manufactured by Matsushita Electric Industrial Co., Ltd. Next, 3 kg of clothes (cotton underwear: 50% by weight, dress shirt made of mixed fabric of polyester/cotton: 50% by weight) were placed thereinto, and thereafter 44.0 g of each detergent composition of Examples was uniformly dispersed. Tap water at 5°C was poured thereinto, and washing was carried out by a setting of "standard course: 3 minutes washing and high water level (66 L)." After termination (without including rinsing step), the amount of the detergent remained in the lint filter was

visually determined by the following evaluation criteria. The water temperature at 5°C was a disadvantageous condition for the dissolubility of the granules, so that the evaluation results A, B and C indicated excellent dissolubility of the granules.

[Evaluation Criteria]

- A: The remnants of the detergent granule being almost zero (estimate number of remained detergent granules: 0 to 5 granules);
- B: No remnant detergent granules (estimate number of remained detergent granules: 6 to 15 granules);
- C: Substantially no remnant detergent granules (estimate number of remained detergent granules: 16 to 30 granules);
- D: The remnants of detergent granules being in small amounts (estimate number of remained detergent granules: 30 to 100 granules);
- E: The remnants of detergent granules being in large amounts (estimate number of remained detergent granules: 101 or more, the remnants of paste being also scattered).

[0030]

Evaluation 2 [Dispersibility of Detergent] The amount 25.0 g of each detergent composition of Examples was placed in an aggregated state near the outer periphery of one of the dents of a sector, a six-divided section of a pulsator of washing machine "AISAIGO NA-F42Y1" manufactured by Matsushita Electric Industrial Co., Ltd. The amount 1.5 kg of the clothes (the same as in Evaluation 1) was placed in the washtub, without disintegrating the agglomeration. Twenty-two liters of tap water at 5°C was poured thereto at a flow rate of 10 L/min such that the water would not directly hit the detergent. After the termination of

water-pouring, the aqueous mixture was allowed to stand. After 3 minutes from the start of water-pouring, the stir was started with gentle water flow (handwashing-mode). After stirring for 3 minutes, water was discharged, and the states of detergents remained on the clothes and the washtub were visually determined by the following evaluation criteria. The stir strength of this evaluation was very weak as compared to that of the standard mode, so that the evaluation criteria I and II indicated excellent dispersibility. In addition, the term "aggregates" described below refers to a mass of aggregated detergent granules having a diameter of 3 mm or more.

[Evaluation Criteria]

- I: No aggregates;
- II: Substantially no aggregates (1 to 5 masses having a diameter of about 3 mm being found);
- III: Aggregates remaining in small amounts (masses having a diameter of about 6 mm being found, and 10 or less masses having a diameter of from 3 to 10 mm being found); and
- IV: Aggregates remaining in large amounts (a large number of masses having a diameter exceeding 6 mm being found).

[0031]

Preparation Example 1 (parts by weight being hereinafter expressed as "parts")

Twenty-five parts of a sodium linear alkyl(10 to 13 carbon atoms)benzenesulfonate; 3 parts of a sodium alkyl(12 to 16 carbon atoms)sulfate; 2 parts of a polyoxyethylene(average moles of EO: 8) alkyl(12 to 14 carbon atoms) ether (hereinafter referred to as "nonionic surfactant"); 3 parts of a soap (14 to 20 carbon atoms); 10 parts of zeolite 4A; 9 parts of No. 1 sodium silicate;

10 parts of sodium carbonate; 2 parts of potassium carbonate; 1.5 parts of sodium sulfate; 0.5 parts of sodium sulfite; 1 part of sodium polyacrylate (average molecular weight: 10,000); 3 parts of an acrylic acid-maleic acid copolymer (Sokalan CP5); 1.5 parts of a polyethylene glycol (average molecular weight: 8,500); and fluorescent dyes (0.1 parts of Tinopal CBS-X and 0.1 parts of WHITEX SA) were mixed with water to prepare a slurry having a solid ingredient of 50% by weight (temperature: 65°C). The resulting slurry was dried by using a countercurrent flow type spray-dryer to give particles having a bulk density of about 300 g/L. The content of volatile matter was 4% (amount lost at 105°C for 2 hours). Subsequently, 78 parts of the granules and 3 parts of zeolite 4A (average particle size: about 3  $\mu\text{m}$ ) were introduced into a High-Speed Mixer (manufactured by Fukae Powtec Corp., volume capacity: 25 L), and mixed. Thereafter, 5 parts of crystalline silicate powders (pulverized product of SKS-6, average particle size: 27  $\mu\text{m}$ ) were introduced into the mixer, and the mixture was further pulverized and granulated with stirring, while spraying 4 parts of the above nonionic surfactant thereto. In this process, 5 parts of the above powdery zeolite was added for surface-coating immediately before the termination of the process, to give base detergent granules (1). The entire charged amount was 5 kg. [0032]

#### Preparation Example 2

Fourteen parts of a potassium linear alkyl(10 to 13 carbon atoms)benzenesulfonate; 8 parts of a sodium salt of methyl ester of  $\alpha$ -sulfofatty acid (14 to 16 carbon atoms); 1 part of the same nonionic surfactant as in Preparation Example 1; 7 parts of the same soap as in Preparation Example 1; 10 parts of zeolite 4A; 1 part of No. 1 sodium silicate; 5 parts of sodium carbonate;

16 parts of potassium carbonate; 1.1 parts of sodium sulfate; 1.5 parts of sodium sulfite; 2 parts of the same sodium polyacrylate as in Preparation Example 1; 2 parts of the same polyethylene glycol as in Preparation Example 1; and fluorescent dyes (0.2 parts of Tinopal CBS-X and 0.1 parts of WHITEX SA) were mixed with water to prepare a slurry having a solid ingredient of 48% by weight (temperature: 65°C). The resulting slurry was dried by using a countercurrent flow type spray-dryer to give particles having a bulk density of about 320 g/L. The content of volatile matter was 3% (amount lost at 105°C for 2 hours). Subsequently, 50 kg/H of the above particles, 4 kg/H of sodium carbonate (heavy ash), 1 kg/H of the same crystalline silicate powders as in Preparation Example 1, and 3 kg/H of the same nonionic surfactant as in Preparation Example 1 were continuously supplied to a continuous kneader (manufactured by Kurimoto Tekkosho K.K.). The resulting mixture was pelletized by using a twin-screw extruder ("PELLETER DOUBLE," manufactured by Fuji Paudal Co., Ltd.) arranged at the discharge outlet of the kneader to give cylindrical pellets having a diameter of about 3 mm. Five parts of powdery zeolite (average particle size: about 3  $\mu$ m) was added as an aid agent for pulverizing, based on 100 parts of the pellets, and the mixture was pulverized and granulated by a Fitz Mill (manufactured by Hosokawa Micron Corporation) equipped with a screen having a 1.5 mm-sieve opening with aeration of cool air at 14°C.

[0033]

#### Preparation Example 3

Twenty-four parts of a sodium linear alkyl(10 to 13 carbon atoms)benzenesulfonate; 4 parts of the same sodium alkylsulfate as in

Preparation Example 1; 4 parts of the same nonionic surfactant as in Preparation Example 1; 1 part of a soap (14 to 20 carbon atoms); 14 parts of No. 1 sodium silicate; 14 parts of sodium carbonate; 4 parts of sodium sulfate; 4 parts of the same acrylic acid-maleic acid copolymer as in Preparation Example 1; 1 part of the same polyethylene glycol as in Preparation Example 1; and fluorescent dyes (0.1 parts of Tinopal CBS-X and 0.1 parts of WHITEX SA) were mixed with water to prepare a slurry having a solid ingredient of 50% by weight (temperature: 63°C). The resulting slurry was dried by using a countercurrent flow type spray-dryer to give particles having a bulk density of about 300 g/L. The content of volatile matter was 2.5% (amount lost at 105°C for 2 hours). Subsequently, 70 parts of the above particles, 7 parts of powdery zeolite (average particle size: about 3  $\mu\text{m}$ ), and 5 parts of the same crystalline silicate as in Preparation Example 1 were blended by using a ribbon blender. The mixture was compressed to regulate its sizes at a roll pressure of about 1 MPa by a Chilsonator (manufactured by Fuji Paudal Co., Ltd., roll width: 102 mm, roll diameter: 254 mm), and the resulting granules were classified with a sieve having a 1,410  $\mu\text{m}$ -sieve opening. The coarse granules of 1,410  $\mu\text{m}$  or more were pulverized by a Fitz Mill using powdery zeolite as an aid agent for pulverizing, and thereafter mixed with sieve-pass granules, to give base detergent granules.

[0034]

#### Preparation Example 4

Fifteen parts of zeolite 4A; 5 parts of sodium sulfate; 2 parts of sodium sulfite; and 2 parts of the same sodium polyacrylate as in Preparation Example 1 were mixed with water to prepare a slurry having a solid ingredient of 50% by

weight (temperature: 58°C). The resulting slurry was spray-dried by using a countercurrent flow type spray-dryer. The content of volatile matter of the particles was 2% (amount lost at 105°C for 2 hours). Twenty parts of the same nonionic surfactant as in Preparation Example 1; 3 parts of the same polyethylene glycol as in Preparation Example 1; and 7 parts of palmitic acid were mixed with heating at 75°C to prepare a liquid mixture. Subsequently, 25 parts of the above particles, 40 parts of crystalline silicate (pulverized product of SKS-6, average particle size: 30 µm), and 5 parts of amorphous aluminosilicate (average particle size: 10 µm, disclosed in Japanese Patent Laid-Open No. Hei 6-179899) were introduced into a Lödige Mixer (manufactured by Matsuzaka Giken Co., Ltd., volume capacity: 20 L, equipped with a jacket), and the stirring with the main shaft (150 rpm) and the chopper (4,000 rpm) was started. The above liquid mixture was supplied to the mixer and was sprayed onto the powder mixture in 2.5 minutes, and thereafter stirred for 6 minutes. Further, 3 parts of the amorphous aluminosilicate was supplied as a surface-coating agent to the mixer, and the mixture was stirred for 1.5 minutes, to give base detergent granules. The entire charged amount was 4 kg.

[0035]

[Classification Procedures for Base Detergent Granules]

Classification procedures were carried out with each of the base detergent granules of Preparation Examples 1 to 4 using the classifier described above. Specifically, 100 g/batch of a sample was first supplied on a 2,000-µm sieve arranged at top of the classifier. Thereafter, the classifier was capped, and attached to a rotating and tapping shaker machine (manufactured by HEIKO SEISAKUSHO, tapping: 156 times/min, rolling: 290 times/min), and vibrated

for 10 minutes. Thereafter, the samples remained on each of the sieves and a receiving tray were individually collected to obtain necessary amounts of samples of each group of the classified granules having sizes of 1,410 to 2,000  $\mu\text{m}$ , 1,000 to 1,410  $\mu\text{m}$ , 710 to 1,000  $\mu\text{m}$ , 500 to 710  $\mu\text{m}$ , 355 to 500  $\mu\text{m}$ , 250 to 355  $\mu\text{m}$ , 180 to 250  $\mu\text{m}$ , 125 to 180  $\mu\text{m}$ , and ones on the tray to 125  $\mu\text{m}$  (less than 125  $\mu\text{m}$ ).

[Classification Procedures for Enzyme Granules]

The same classification procedures as those of the base detergent granules were carried out for Enzyme Granules A (manufactured by NOVO Nordisk, Savinase 18T Type W), to give each of the classified enzyme granules.

[Determination of Dissolving Rate  $V_i$  of Each of Classified Granules]

The dissolving rate of each group of the classified granules was determined in accordance with the determination method described above. The results are shown in Table 1.

[0036]



[Table 1]

Vi	Prep. Ex.1	Prep. Ex.2	Prep. Ex.3	Prep. Ex.4	Enzyme A
V [1410-2000 $\mu$ m]	44.8	48.2	44.5	59.9	-
V [1000-1410 $\mu$ m]	53.8	58.9	54.6	70.5	59.4
V [710-1000 $\mu$ m]	64.1	67.8	61.5	84.3	74.4
V [500- 710 $\mu$ m]	77.6	82.3	78.3	97.6	81.3
V [355- 500 $\mu$ m]	95.4	98.2	96.8	99.7	95.0
V [250- 355 $\mu$ m]	99.6	99.6	99.5	99.8	99.7
V [180- 250 $\mu$ m]	100	100	100	100	-
V [125- 180 $\mu$ m]	100	100	100	100	-
V [Less than 125 $\mu$ m]	100	100	100	100	-

[0037]

Example 1

Detergent compositions were obtained using the classified granules of the base detergent granules of Preparation Examples 1 to 4, Enzyme Granules A by adjusting particle size distribution in accordance with the following process.

Operation 1 for Adjusting Particle Size Distribution

Each of the classified granules was weighed so that each sample weighs 200 g in accordance with a mass base frequency distribution of the particle size shown in Table 2, and each sample was mixed for 2 minutes by a rocking mixer (manufactured by Aichi Electronics Co., Ltd.) to prepare various detergent compositions of which particle size was adjusted.

The detergent compositions shown in Table 2 were evaluated in accordance with the Evaluations 1 and 2. As a result, in the detergent compositions I (Examples 1 to 9), it has been found that Examples 1, 4, 5, and 6 satisfying the formula (A) of  $\sum (W_i \cdot V_i) \geq 95(\%)$  and having a mass base frequency of the classified granules having sizes of less than 125  $\mu\text{m}$  of 0.1 or less were excellent in the dissolubility and the dispersibility. Also, in the detergent compositions II (Examples 10 and 11), it has been found that Example 10 satisfying the formula (B) of  $\sum (W_i \cdot V_i) \geq 97(\%)$  and having a mass base frequency of the classified granules having sizes of less than 125  $\mu\text{m}$  of 0.08 or less were excellent in the dissolubility and the dispersibility.

[0038]

[Table 2]

Base Detergent Granules Used	Ex.1	Ex.2	Ex.3	Ex.4		Ex.5	Ex.6	Ex.7
	Prep. Ex.1	Prep. Ex.1	Prep. Ex.1	Prep. Ex.1	Enzyme A	Prep. Ex.2	Prep. Ex.2	Prep. Ex.2
W [1410-2000 $\mu$ m]	0.00	0.01	0.00	0.00	0.00	0.01	0.01	0.00
W [1000-1410 $\mu$ m]	0.00	0.02	0.00	0.00	0.00	0.02	0.10	0.00
W [710-1000 $\mu$ m]	0.00	0.06	0.00	0.01	0.01	0.06	0.22	0.02
W [500- 710 $\mu$ m]	0.01	0.07	0.02	0.04	0.02	0.07	0.26	0.03
W [355- 500 $\mu$ m]	0.13	0.16	0.07	0.21	0.00	0.16	0.17	0.11
W [250- 355 $\mu$ m]	0.40	0.40	0.14	0.33	0.00	0.40	0.11	0.18
W [180- 250 $\mu$ m]	0.40	0.18	0.28	0.31	0.00	0.18	0.06	0.24
W [125- 180 $\mu$ m]	0.04	0.08	0.33	0.04	0.00	0.08	0.04	0.26
W [Less than 125 $\mu$ m]	0.02	0.02	0.16	0.03	0.00	0.02	0.03	0.16
Average Particle Size [ $\mu$ m]	259	303	182	284		303	565	201
Bulk Density [g/L]	773	770	731	775		839		
Flowability [sec]	6.3	6.8	UD	6.4		6.4 UD		
$\Sigma$ (Wi•VI) [%]	99.0	93.9	99.3	97.0		95.0	83.3	98.6
Evaluation 1	A	C	A	A-B		B	D	A
Evaluation 2	I	II	IV	I		II	I	IV

Note: UD means undeterminable.

- Continued -

- Continued -

Base Detergent Granules Used	Ex.8	Ex.9	Ex.10	Ex.11
	Prep. Ex.3	Prep. Ex.3	Prep. Ex.4	Prep. Ex.4
W [1410-2000 $\mu$ m]	0.00	0.00	0.00	0.00
W [1000-1410 $\mu$ m]	0.00	0.09	0.00	0.04
W [710-1000 $\mu$ m]	0.04	0.20	0.03	0.14
W [500- 710 $\mu$ m]	0.09	0.19	0.10	0.15
W [355- 500 $\mu$ m]	0.25	0.14	0.26	0.16
W [250- 355 $\mu$ m]	0.23	0.12	0.30	0.16
W [180- 250 $\mu$ m]	0.19	0.08	0.21	0.13
W [125- 180 $\mu$ m]	0.10	0.08	0.08	0.13
W [Less than 125 $\mu$ m]	0.10	0.10	0.02	0.09
Average Particle Size [ $\mu$ m]	296	476	312	347
Bulk Density [g/L]		769		890
Flowability [sec]		6.9		6.1
$\Sigma$ (Wi•Vi) [%]	95.6	83.6	99.2	96.2
Evaluation 1	B	D	A	B
Evaluation 2	II	II	II	IV

[0039]

Example 2

Each of the high-density detergent compositions was obtained using the classified granules of the base detergent granules (1) of Preparation Example 1 by adjusting particle size distribution in accordance with the following process.

Operation 2 for Adjusting Particle Size Distribution

One-hundred parts of the base detergent granules (1) obtained in Preparation Example 1 were classified by a gyratory screen (manufactured by Tokuju Kosakusho) having a screen having a 500  $\mu\text{m}$ -sieve opening. The sieve-on granules were removed to give 55.3 parts of the detergent composition of Example 12.

Operation 3 for Adjusting Particle Size Distribution

The amount 55.3 parts of the detergent composition of Example 12 was introduced as base detergent granules into a gyratory screen having a screen having a 125  $\mu\text{m}$ -sieve opening to remove fine powder having a size of less than 125  $\mu\text{m}$ , thereby giving 51.5 parts of the detergent composition of Example 13.

[0040]

Operation 4 for Adjusting Particle Size Distribution

In the same manner as in Operation 2 for adjusting particle size distribution, 100 parts of the base detergent granules (1) obtained in Preparation Example 1 were introduced into a gyratory screen having a screen having a 500  $\mu\text{m}$ -sieve opening, and classified into sieve-on granules A and sieve-pass granules A, wherein the weights thereof were 44.7 parts and 55.3 parts, respectively. The amount 44.7 parts of the sieve-on granules A and 2 parts of powdery zeolite (average particle size: 3  $\mu\text{m}$ ) as an aid agent for pulverization

were fed into a Fitz Mill (manufactured by Hosokawa Micron Corporation) with cooling air, to give a first-step pulverized granules. Thereafter, the first-step pulverized granules were fed into the second step of the Fitz Mill to give second-step pulverized granules. The opening of the screen of the Fitz Mill for the first-step had a diameter of 2 mm and that for the second-step had a diameter of 1 mm. The average particle size of the second-step pulverized granules was 376  $\mu\text{m}$ . Of the 48.7 parts of the second-step pulverized granules, granules having a size of 500  $\mu\text{m}$  or more occupied 23.2 parts. The second-step pulverized granules were introduced into the above gyratory screen having a screen having a 500  $\mu\text{m}$ -sieve opening, and classified into sieve-on granules B and sieve-pass granules B. The amount 25.5 parts of sieve-pass granules B and 55.3 parts of the sieve-pass granules A were blended to give 80.8 parts of the detergent composition of Example 14.

[0041]

#### Operation 5 for Adjusting Particle Size Distribution

The amount 80.8 parts of the detergent composition of Example 14 was introduced into the above gyratory screen having a screen having a 125  $\mu\text{m}$ -sieve opening to remove fine powder having a size of less than 125  $\mu\text{m}$ , thereby giving 76.0 parts of the detergent composition of Example 15.

[0042]

#### Operation 6 for Adjusting Particle Size Distribution

The amount 80.8 parts of the detergent composition of Example 14 was introduced into a gyratory screen having a screen having a 180  $\mu\text{m}$ -sieve opening, and classified into sieve-on granules C and sieve-pass granules C. The weights of the sieve-on granules C and the sieve-pass granules C were 65.4 parts and

15.4 parts, respectively.

[0043]

The sieve-pass granules C were granulated according to the following procedures. The amount 15.4 parts of the sieve-pass granules C was introduced into the above High-Speed Mixer, and 0.77 parts of the above nonionic surfactant was sprayed thereto over a period of 1.3 minutes. Thereafter, the mixture was granulated with stirring for 10 minutes. Subsequently, the resulting granules were subjected to a surface-coating treatment for 1 minute by adding 0.92 parts of zeolite (average particle size: about 3  $\mu\text{m}$ ), to give base detergent granules (2) (average particle size: 662  $\mu\text{m}$ ). The base detergent granules were classified into sieve-on granules A' and sieve-pass granules A' using a gyratory screen having a 500  $\mu\text{m}$ -sieve opening. The sieve-on granules A' were subjected to two-step pulverizing using a Fitz Mill to classify the resulting pulverized granules into sieve-on granules B' and sieve-pass granules B' using a gyratory screen having a 500  $\mu\text{m}$ -sieve opening. Thereafter, the sieve-pass granules B', the sieve-pass granules A' and the sieve-pass granules C were blended to give 80.0 parts of the detergent composition of Example 16.

Each of the detergent compositions shown in Table 3 was evaluated in accordance with the Evaluations 1 and 2. As a result, it has been found that Examples 12 to 16 were excellent in the dissolubility and the dispersibility. Here, it has been found that Examples 13, 15, and 16 having a low mass base frequency of the classified granules having sizes of less than 125  $\mu\text{m}$  were particularly excellent in the dispersibility.

[0044]

[Table 3]

Base Detergent Granules Used	Ex.12	Ex.13	Ex.14	Ex.15	Ex.16
	Prep. Ex. 1	Prep. Ex. 1	Prep. Ex. 1	Prep. Ex. 1	Prep. Ex. 1
W [1410-2000 $\mu\text{m}$ ]	0.00	0.00	0.00	0.00	0.00
W [1000-1410 $\mu\text{m}$ ]	0.00	0.00	0.00	0.00	0.00
W [710-1000 $\mu\text{m}$ ]	0.00	0.00	0.00	0.00	0.00
W [500- 710 $\mu\text{m}$ ]	0.00	0.00	0.00	0.00	0.00
W [355- 500 $\mu\text{m}$ ]	0.14	0.15	0.30	0.30	0.30
W [250- 355 $\mu\text{m}$ ]	0.31	0.34	0.28	0.32	0.36
W [180- 250 $\mu\text{m}$ ]	0.31	0.33	0.24	0.24	0.29
W [125- 180 $\mu\text{m}$ ]	0.17	0.18	0.13	0.14	0.04
W [Less than 125 $\mu\text{m}$ ]	0.07	0.00	0.05	0.00	0.01
Average Particle Size [ $\mu\text{m}$ ]	237	248	276	285	292
Bulk Density [g/L]	701	730	715	708	704
Flowability [sec]	7.3	6.5	6.7	6.2	6.3
$\Sigma (W_i \cdot V_i)$ [%]	99.2	99.2	98.5	98.5	98.5
Evaluation 1	A	A	A	A	A
Evaluation 2	II	I	I	I	I



[0045]

[Effects of the Invention]

The detergent composition of the present invention rapidly dissolves after supplying to water, even with cold water, is excellent in the dispersibility owing to agglomeration of the granules, and is excellent in dissolubility and detergency under washing conditions of low-mechanical power as employed in recent washing machines.

[Brief Description of the Drawings]

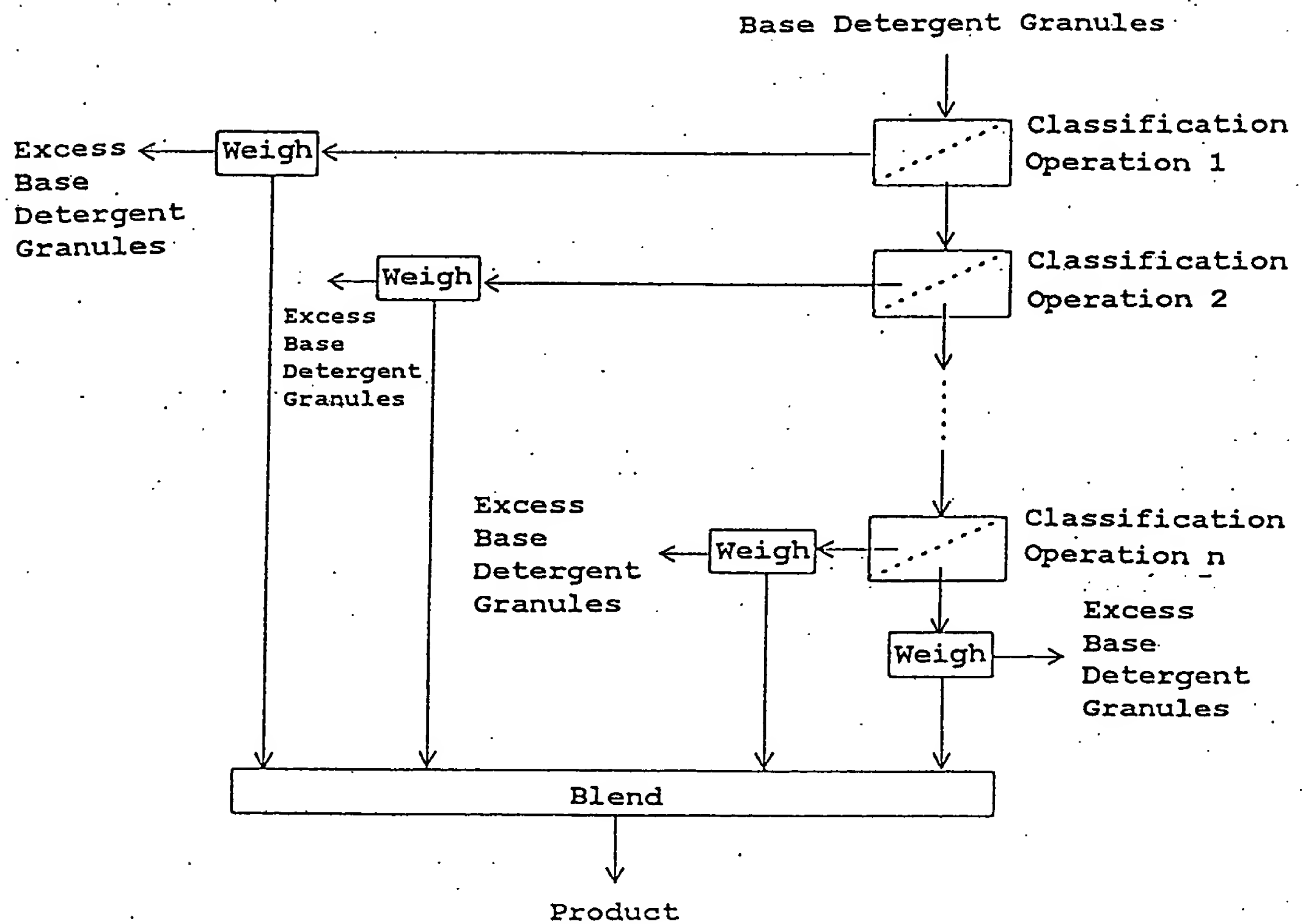
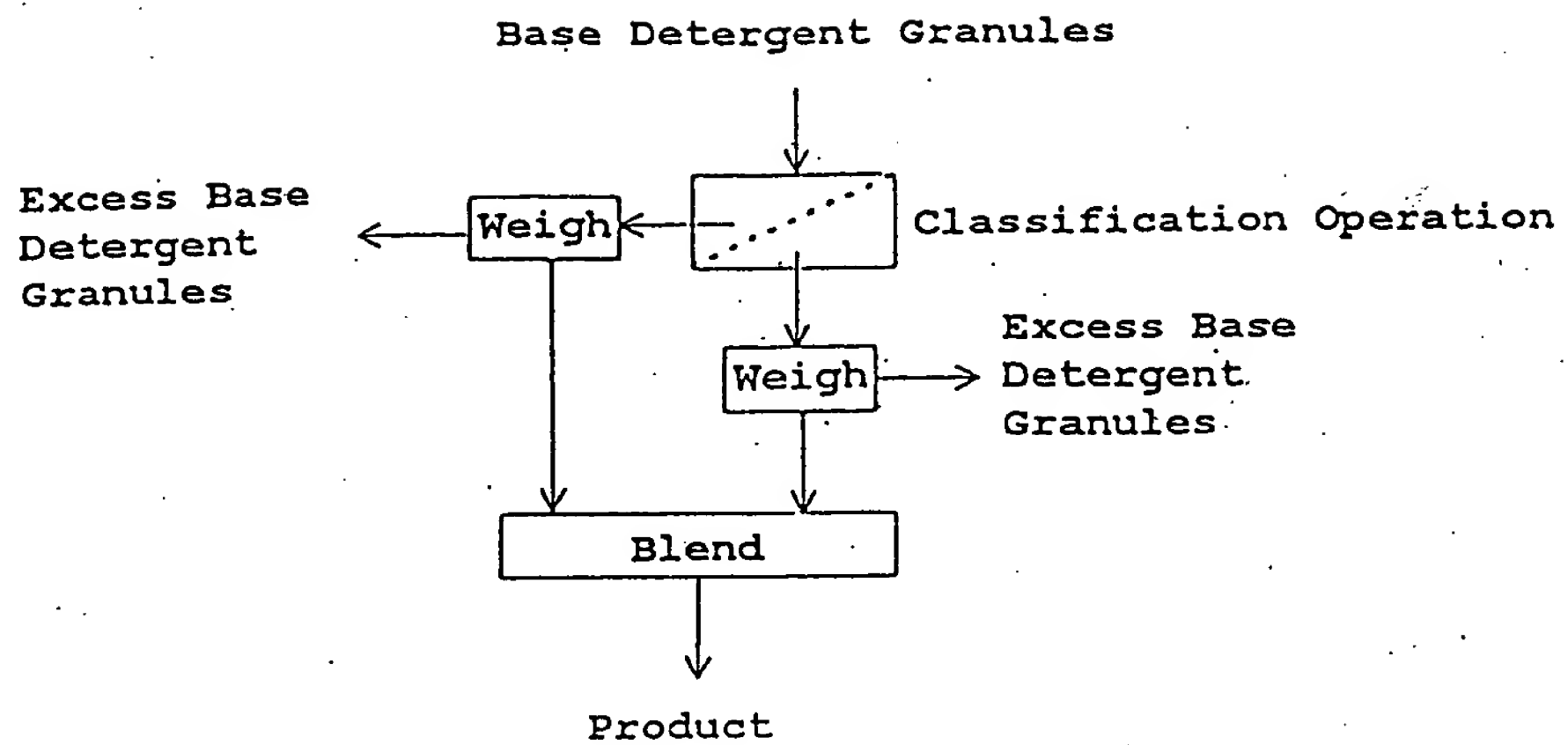
[Figure 1]

Figure 1 (1) and (2) each shows a scheme of classification operation in the process of the present invention.

[Document]

Drawings

[Figure 1]



[Document] Abstract

[Abstract]

[Problems]

To provide a high-density detergent composition which is excellent in the detergency even when the amount of work of the washing machine is low, excellent in the dissolubility of granules and the dispersibility.

[Solving Means]

A high-density detergent composition comprising 10 to 60% by weight of a surfactant composition having a weight ratio of an anionic surfactant to a nonionic surfactant of 4:10 or more and 10:0 or less, wherein the high-density detergent composition has a total summation of a product of a mass base frequency  $W_i$  and a dissolving rate  $V_i$  of each group of classified granules obtained by classifying detergent granules, which satisfies the following formula:  $\Sigma(W_i \bullet V_i) \geq 95(\%)$ , and wherein a mass base frequency of the classified granules having a size of less than 125  $\mu\text{m}$  is 0.1 or less.

[Selected Drawings] None